

ChE/MSE 505
Advanced Mathematic for Engineers
Final Exam
Fall Semester, 2004
Instructor: David Keffer
Administered: 8:00-10:00 am, Wednesday December 8, 2004

Problem 1.

Consider the partial differential equation describing the steady-state temperature profile in an uninsulated cylindrical metal rod of radius R and length L , in which there is variation in the radial (r) and axial (z) directions only. The two axial ends of the rod are held at fixed temperatures.

$$0 = \alpha \nabla^2 T \tag{1}$$

where α is the thermal diffusivity. The Laplacian in two-dimensional cylindrical coordinates is defined as

$$\nabla^2 T = \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{\partial^2 T}{\partial z^2}. \tag{2}$$

You may need the following properties: h is the heat transfer coefficient, ρ is the density, C_p is the heat capacity, k_c is the thermal conductivity, and T_{surr} is the temperature of the surroundings.

- (a) Categorize the type of PDE: parabolic, hyperbolic, or elliptic.
- (b) Determine the linearity of the PDE.
- (c) Specify a complete set of consistent initial and boundary conditions for this problem.
- (d) Identify and provide a detailed algorithm describing a numerical technique suitable for the solution of this problem.

Solution:

- (a) Categorize the type of PDE: parabolic, hyperbolic, or elliptic.

The PDE is elliptic. There is no time derivative of any order in it.

- (b) Determine the linearity of the PDE.

The PDE is linear in the unknown, T .

- (c) Specify a complete set of consistent initial and boundary conditions for this problem.

There are no initial conditions for an elliptic PDE.

A complete set of consistent boundary conditions are

$$\begin{aligned}
T(z = 0, r) &= T_o && \text{(Temperature is fixed at axial end 1.)} \\
T(z = L, r) &= T_f && \text{(Temperature is fixed at axial end 1.)} \\
\left. \frac{\partial T}{\partial r} \right|_{r=0} &= 0 && \text{(Radial symmetry.)} \\
\frac{q}{A} &= h(T(z, r = R) - T_{surr}) = -k_c \left. \frac{\partial T}{\partial r} \right|_{r=R} && \text{(Uninsulated boundary, flux is heat lost.)}
\end{aligned}$$

(d) Identify and provide a detailed algorithm describing a numerical technique suitable for the solution of this problem.

For solving a linear elliptic PDE, we first discretize r and z directions. Then for each point in r, z space, we can write an equation of the form:

$$\begin{aligned}
0 &= \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{\partial^2 T}{\partial z^2} = \frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{\partial^2 T}{\partial z^2} \\
0 &= \left(\frac{T_{i+1,j} - 2T_{i,j} + T_{i-1,j}}{\Delta r^2} \right) + \frac{1}{r_{i,j}} \left(\frac{T_{i+1,j} - T_{i-1,j}}{\Delta r} \right) + \left(\frac{T_{i,j+1} - 2T_{i,j} + T_{i,j-1}}{\Delta z^2} \right).
\end{aligned}$$

If we have n_r intervals in the r direction and n_z intervals in the z direction, then we are going to have $n_r n_z$ equations of this form. They will comprise a system of linear algebraic equations. We can solve them using linear algebra.

Problem 2.

If the cylinder in problem 1 also loses heat to the surroundings via radiation, we must add an additional term to the energy balance in equation (1),

$$0 = \alpha \nabla^2 T - \frac{2\varepsilon\sigma}{R\rho C_p} (T^4 - T_{surr}^4) \tag{3}$$

where ε is the total emissivity of the cylinder and σ is a proportionality constant.

(e) Determine the linearity of the PDE.

(f) Identify and provide a detailed algorithm describing a numerical technique suitable for the solution of this problem.

Solution

(e) Determine the linearity of the PDE.

The PDE is now nonlinear.

(f) Identify and provide a detailed algorithm describing a numerical technique suitable for the solution of this problem.

For solving a nonlinear elliptic PDE, we first discretize r and z directions as we did for the linear case. Then for each point in r,z space, we can write an equation of the form:

$$0 = \left(\frac{T_{i+1,j} - 2T_{i,j} + T_{i-1,j}}{\Delta r^2} \right) + \frac{1}{r_{i,j}} \left(\frac{T_{i+1,j} - T_{i-1,j}}{\Delta r} \right) + \left(\frac{T_{i,j+1} - 2T_{i,j} + T_{i,j-1}}{\Delta z^2} \right) - \frac{2\varepsilon\sigma}{\alpha R \rho C_p} (T_{i,j}^4 - T_{surr}^4)$$

If we have n_r intervals in the r direction and n_z intervals in the z direction, then we are going to have $n_r n_z$ equations of this form. They will comprise a system of nonlinear algebraic equations. We can solve them using the Newton-Raphson method. If we have a hard time getting an initial guess, we can insert a parameter, ζ in front of the radiation term. We can parameter step through ζ from 0 to 1, using the converged solution from the previous value of ζ as an initial guess for the next value of ζ . The first initial guess will come from the solution of the linear problem when $\zeta = 0$.

Problem 3.

We want to use the following equation to fit some vapor pressure data.

$$P^{vap} = \exp\left(\frac{A}{B+T}\right) \quad (4)$$

where T is temperature and A and B are fitting constants. We have two pieces of data: the vapor pressure at 300 K is 1.1 atm and the vapor pressure at 320 K is 1.7 atm. Given this experimental data find the best values of A and B .

Solution:

We have two unknowns A and B . Our life would be much simpler if we can rearrange the problem so that it is linear in A and B . Let's try.

$$(B+T)\ln(P^{vap}) - A = 0$$

There we have it. The equation is linear in A and B . We have a system of two linear equations and two unknowns.

$$\begin{aligned} f_1(A, B) &= (B+T_1)\ln(P_1^{vap}) - A \\ f_2(A, B) &= (B+T_2)\ln(P_2^{vap}) - A \end{aligned}$$

We can write this in matrix notation as

$$\underline{\mathbf{J}}\underline{\mathbf{x}} = \underline{\mathbf{R}}$$

where

$$\underline{\underline{\mathbf{J}}} = \begin{bmatrix} -1 & \ln(P_1^{vap}) \\ -1 & \ln(P_2^{vap}) \end{bmatrix}, \quad \underline{\underline{\mathbf{x}}} = \begin{bmatrix} A \\ B \end{bmatrix}, \quad \text{and} \quad \underline{\underline{\mathbf{R}}} = \begin{bmatrix} -T_1 \ln(P_1^{vap}) \\ -T_2 \ln(P_2^{vap}) \end{bmatrix}$$

We need the determinant and inverse

$$\det(\underline{\underline{\mathbf{J}}}) = -\ln(P_2^{vap}) + \ln(P_1^{vap}) = \ln\left(\frac{P_1^{vap}}{P_2^{vap}}\right)$$

$$\underline{\underline{\mathbf{J}}}^{-1} = \frac{1}{\det(\underline{\underline{\mathbf{J}}})} \begin{bmatrix} j_{22} & -j_{12} \\ -j_{21} & j_{11} \end{bmatrix} = \frac{1}{\ln\left(\frac{P_1^{vap}}{P_2^{vap}}\right)} \begin{bmatrix} \ln(P_2^{vap}) & -\ln(P_1^{vap}) \\ 1 & -1 \end{bmatrix}$$

The solution is given by

$$\underline{\underline{\mathbf{x}}} = \underline{\underline{\mathbf{J}}}^{-1} \underline{\underline{\mathbf{R}}} = \frac{1}{\ln\left(\frac{P_1^{vap}}{P_2^{vap}}\right)} \begin{bmatrix} \ln(P_2^{vap}) & -\ln(P_1^{vap}) \\ 1 & -1 \end{bmatrix} \begin{bmatrix} -T_1 \ln(P_1^{vap}) \\ -T_2 \ln(P_2^{vap}) \end{bmatrix} = \frac{1}{\ln\left(\frac{P_1^{vap}}{P_2^{vap}}\right)} \begin{bmatrix} (T_2 - T_1) \ln(P_1^{vap}) \ln(P_2^{vap}) \\ -T_1 \ln(P_1^{vap}) + T_2 \ln(P_2^{vap}) \end{bmatrix}$$

We have two pieces of data: the vapor pressure at 300 K is 1.1 atm and the vapor pressure at 320 K is 1.7 atm.

$$\underline{\underline{\mathbf{x}}} = \frac{1}{\ln\left(\frac{1.1}{1.7}\right)} \begin{bmatrix} 20 \ln(1.1) \ln(1.7) \\ -300 \ln(1.1) + 320 \ln(1.7) \end{bmatrix} \approx -2.2972 \begin{bmatrix} 1.0115 \\ 141.21 \end{bmatrix} = \begin{bmatrix} -2.3236 \\ -324.38 \end{bmatrix}$$