

CBE 450 Chemical Reactor Fundamentals
Fall, 2009
Homework Assignment #3

1. Numerical Solution of a Single Nonlinear Algebraic Equation

Consider a continuous stirred-tank reactor (CSTR) in which the following dimerization reaction goes from $2A \rightarrow B$ with the following mass balance on A at steady state

$$\text{accumulation} = \text{in} - \text{out} + \text{generation}$$

$$0 = F_{in} C_{A,in} - F_{out} C_A - V k_{dimer} C_A^2$$

The inlet flow rate is 1 liter/sec, as is the outlet flow rate. The inlet concentration is 10 mole/liter. The rate constant is 0.5 liter/mol²/sec. The volume of the reactor is 1 liter.

- (a) Solve this nonlinear equation analytically.
- (b) How many roots are there?
- (c) Which root is the physically meaningful root? Why?
- (d) Solve this nonlinear equation using Goalseek in Excel. Provide a print-out of the spreadsheet.
- (e) Solve this nonlinear equation using the Newton-Raphson method with numerical derivatives in Matlab. Note the initial guess you used to converge to the physically meaningful root.

2. Numerical Solution of a System of Nonlinear Algebraic Equations

Consider a continuous stirred-tank reactor (CSTR) in which the following isomerization reaction goes from $A \rightarrow B$ with the following mass balance on A at steady state

$$\text{accumulation} = \text{in} - \text{out} + \text{generation}$$

$$0 = F_{in} C_{A,in} - F_{out} C_A - V k_{iso} C_A$$

The inlet flow rate is 1 liter/sec, as is the outlet flow rate. The inlet concentration is 10 mole/liter. The rate constant is

$$k_{iso} = k_o \exp\left(-\frac{E_a}{RT}\right)$$

where $k_o = 1.0 \text{ sec}^{-1}$ and $E_a = 2500 \text{ J/mol/K}$. The volume of the reactor is 1 liter.

The steady state energy balance is

$$\text{accumulation} = \text{in} - \text{out} + \text{generation}$$

$$0 = F_{in} H_{in} - F_{out} H - \Delta H_R V k_{iso} C_A$$

where the inlet enthalpy, $H_{in} = C_p T_{in}$, where the heat capacity is 4.0 kJ/liter/K and the inlet temperature is 300 K, where the enthalpy of the reactor is $H = C_p T$, and where the heat of reaction, ΔH_R , is -30 kJ/mol.

Find the steady state concentration of A and temperature. Provide Matlab equation input file and screen output. (You do not have to provide the entire Newton-Raphson code provided in class.)

3. Numerical Solution of a System of Nonlinear Ordinary Differential Equations

Consider a continuous stirred-tank reactor (CSTR) in which the following isomerization reaction goes from A \rightarrow B with the following mass balance on A

$$\text{accumulation} = \text{in} - \text{out} + \text{generation}$$

$$V \frac{dC_A}{dt} = F_{in} C_{A,in} - F_{out} C_A - V k_{iso} C_A$$

The inlet flow rate is 1 liter/sec, as is the outlet flow rate. The inlet concentration is 10 mole/liter. The rate constant is

$$k_{iso} = k_o \exp\left(-\frac{E_a}{RT}\right)$$

where $k_o = 1.0 \text{ sec}^{-1}$ and $E_a = 2500 \text{ J/mol/K}$. The volume of the reactor is 1 liter.

The energy balance is

$$\text{accumulation} = \text{in} - \text{out} + \text{generation}$$

$$V C_p \frac{dT}{dt} = F_{in} H_{in} - F_{out} H - \Delta H_R V k_{iso} C_A$$

where the inlet enthalpy, $H_{in} = C_p T_{in}$, where the heat capacity is 4.0 kJ/liter/K and the inlet temperature is 300 K, where the enthalpy of the reactor is $H = C_p T$, and where the heat of reaction, ΔH_R , is -30 kJ/mol.

The initial conditions within the reactor are $T(t=0) = 300 \text{ K}$ and $C_A(t=0) = 0.0 \text{ mol/liter}$.

- (a) Find the transient behavior of the concentration and temperature. Provide the Matlab equation input file and graphical output. (You do not have to provide the entire Runge-Kutta code provided in class.)
- (b) What are the long-time (steady state values) of the concentration of A and the temperature?
- (c) How do the values in (b) compare with the steady state solutions obtained in problem 2?